

Studies on densities and viscosities of binary mixtures of alkyl benzoates in *n*-heptane

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Abstract

Densities and viscosities have been determined for the two binary mixtures of methyl and ethyl benzoate in *n*-heptane at different concentrations and temperatures. The corresponding excess properties and the activation magnitudes were also calculated from the experimental data. All excess properties, including the excess Gibbs free energy of activation of flow, are negative over the entire range of compositions. The results for these binary mixtures are compared with those for methyl benzoate with *n*-nonane, the molecular interactions occurring in the mixtures being explained on the basis of the deviation from ideality of the magnitudes studied.

INTRODUCTION

This paper is part of a broad program of research into the thermodynamic behavior of mixtures of esters and various solvents (*n*-alkanes, *n*-alcohols, and 1-chloroalkanes) that has been in progress at our laboratory for some time. The study of such behavior has so far been concerned with the different mixing properties, h^E , g^E , v^E , and the VLE values, for binary systems composed of aliphatic esters and a second component. The results have indicated the existence of specific interactions caused by the presence of the $-\text{COO}-$ group. However, an earlier paper [1] which reported an initial study on the v^E , η^E and Δg^{*E} values of aromatic esters for the binary system methyl benzoate + *n*-nonane, did not consider this aspect. This paper, therefore, investigates the special behavior of the ester group on the benzene ring, using magnitudes that do not generate thermal effects, i.e. as if the large size of the benzoate molecule was the primary cause of the

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discrepancy with respect to the ideal behavior of the systems that contain them.

This second paper thus presents direct experimental values for density ρ and viscosity η , and indirect values for the excess magnitudes for the two binary systems methyl benzoate + *n*-heptane and ethyl benzoate + *n*-heptane at four temperatures between 288.15 and 318.5 K. The thermodynamic activation functions that complete this study were calculated from the variation in ρ and η with temperature.

The v^E values at 298.15 K for the two mixtures considered here, were found in the literature [2, 3] and will be used for purposes of comparison.

EXPERIMENTAL

The density ρ and viscosity η values for the pure components and their mixtures were measured respectively in an Anton Paar 60/602 digital densimeter and in a Cannon–Fenske viscosimeter; the operation and calibration of these instruments were described in a previous paper [1]. The accuracy of the direct measurements of ρ was $\pm 0.002 \text{ kg m}^{-3}$ and that of η , $\pm 0.003 \text{ mPa s}$. The precision of the magnitudes calculated indirectly was: for the concentrations x , $\pm 5 \times 10^{-5}$; for the excess volumes v^E , $\pm 2 \times 10^{-9} \text{ m}^3 \text{ mol}^{-1}$; and for the excess viscosities η^E , $\pm 0.005 \text{ mPa s}$.

The components used in the present study did not undergo any further purification but were simply degassed ultrasonically for several hours and then dried in darkness on a molecular sieve (Fluka) prior to use. The *n*-heptane (puriss. p.a. >99.5 mol.%) was supplied by Fluka; the alkyl benzoates (+99 mol.%) were from Aldrich. Table 1 gives the values recorded for the most important properties of the components used in this experiment and also the values compiled from the literature for comparison. Even though the properties for methyl benzoate (Fluka) were reported in an earlier paper [1], the values were redetermined experimentally here because this time it was purchased from a different manufacturer. Using the expression $\alpha = -(\partial \ln \rho / \partial T)_p$, the mean coefficients of thermal expansion were also calculated from the density values at temperatures in the range 288.15–318.15 K. On the whole, the agreement between our experimental data and the literature values was good, with maximum errors of less than 4%.

RESULTS

The experimental data for density ρ and dynamic viscosity η for the mixtures $x_1 \text{C}_6\text{H}_5\text{COOC}_u\text{H}_{2u+1} + x_2 n\text{-C}_7\text{H}_{16}$, where u is 1 or 2, at different concentrations and temperatures are given in Table 2, which also contains the excess values for the molar volumes, for the viscosity calculated using a non-logarithmic equation, and for the free activation energy of the viscous

TABLE 1

Properties of pure compounds at different temperatures and their comparison with literature data

Property	288.15 K		298.15 K		308.15 K		318.15 K	
	Exp.	Lit.	Exp.	Lit.	Exp.	Lit.	Exp.	Lit.
<i>n</i> -Heptane								
n_D	1.3903		1.3854	1.3851 [4] 1.3855 [5]	1.3805	1.3802 [5]	1.3755	1.3750 [5]
ρ /(kg m ⁻³)	689.46		679.28	679.46 [4, 6] 679.52 [5] 679.37 [7]	670.62	671.07 [5]	661.92	662.32 [5]
η /(mPa s)	0.441	0.441 [4] 0.440 [6]	0.394	0.397 [4] 0.395 [6] 0.388 [7]	0.353	0.3592 [4] 0.3581 [6]	0.318	0.326 [6]
α /(K ⁻¹)	0.00134	0.00124 [4]						
Methyl benzoate								
n_D	1.5192	1.5190 [1]	1.5145	1.51457 [4] 1.5144 [1]	1.5101	1.5102 [1]	1.5058	1.5056 [1]
ρ /(kg m ⁻³)	1092.62	1093.34 [4] 1091.85 [1]	1083.60	1083.52 [1]	1074.07	1073.29 [1]	1064.52	1063.50 [1]
η /(mPa s)	2.246	2.298 [4] 2.250 [1]	1.793	1.809 [1]	1.485	1.476 [1]	1.232	1.224 [1]
α /(K ⁻¹)	0.00087	0.000876 [4]						
Ethyl benzoate								
n_D	1.5071	1.50748 [4]	1.5026	1.50348 [4]	1.4985		1.4940	
ρ /(kg m ⁻³)	1050.42	1051.12 [4]	1041.63	1042.1 [7]	1032.55		1023.00	
η /(mPa s)	2.394	2.407 [4]	1.906	1.990 [7]	1.560		1.294	
α /(K ⁻¹)	0.00088	0.00089 (293.15 K) [4]						

TABLE 2

Densities ρ viscosities η and excess properties for the systems x_1 methyl (or ethyl) benzoate + x_2 *n*-heptane at several temperatures

x_1	$\rho/(\text{kg m}^{-3})$	$v^E \times 10^6/(\text{m}^3 \text{mol}^{-1})$	$\eta/(\text{mPa s})$	$\eta^E/(\text{mPa s})$	$\Delta g^{*E}/(\text{kJ mol}^{-1})$
Methyl benzoate(1) + <i>n</i> -heptane(2)					
288.15 K					
0.9017	1048.6	-0.173	1.777	-0.291	-0.178
0.8033	1005.2	-0.274	1.434	-0.456	-0.308
0.6984	959.9	-0.315	1.149	-0.553	-0.430
0.5987	917.4	-0.305	0.950	-0.570	-0.491
0.5004	877.5	-0.262	0.814	-0.530	-0.482
0.3974	836.2	-0.195	0.690	-0.468	-0.475
0.3001	798.5	-0.124	0.607	-0.375	-0.400
0.1960	759.4	-0.056	0.528	-0.267	-0.332
0.0999	724.5	-0.012	0.480	-0.142	-0.187
298.15 K					
0.9017	1039.4	-0.204	1.435	-0.221	-0.184
0.8033	995.8	-0.323	1.183	-0.335	-0.293
0.6984	950.2	-0.373	0.968	-0.403	-0.396
0.5978	907.6	-0.365	0.814	-0.416	-0.446
0.5004	867.4	-0.320	0.701	-0.393	-0.449
0.3974	826.1	-0.247	0.601	-0.349	-0.444
0.3001	788.3	-0.169	0.533	-0.282	-0.379
0.1960	749.2	-0.089	0.464	-0.204	-0.329
0.0999	714.3	-0.032	0.425	-0.109	-0.187
308.15 K					
0.9017	1030.0	-0.236	1.197	-0.176	-0.190
0.8033	986.3	-0.346	1.008	-0.254	-0.269
0.6984	940.9	-0.411	0.839	-0.305	-0.353
0.5978	898.4	-0.420	0.708	-0.322	-0.418
0.5004	858.3	-0.382	0.616	-0.303	-0.414
0.3974	817.1	-0.303	0.535	-0.267	-0.393
0.3001	779.4	-0.210	0.472	-0.221	-0.358
0.1960	740.3	-0.112	0.418	-0.156	-0.283
0.0999	705.5	-0.039	0.382	-0.084	-0.163
318.15 K					
0.9017	1020.6	-0.262	1.024	-0.118	-0.139
0.8033	976.9	-0.385	0.860	-0.193	-0.250
0.6984	931.5	-0.457	0.720	-0.238	-0.341
0.5978	889.4	-0.469	0.620	-0.245	-0.379
0.5004	849.1	-0.430	0.539	-0.236	-0.395
0.3974	808.0	-0.349	0.475	-0.207	-0.364
0.3001	770.4	-0.250	0.422	-0.171	-0.328
0.1960	731.4	-0.142	0.378	-0.120	-0.247
0.0999	696.7	-0.057	0.346	-0.064	-0.138

TABLE 2 (continued)

x_1	$\rho/(\text{kg m}^{-3})$	$v^E \times 10^6/(\text{m}^3 \text{mol}^{-1})$	$\eta/(\text{mPa s})$	$\eta^E/(\text{mPa s})$	$\Delta g^{*E}/(\text{kJ mol}^{-1})$
Ethyl benzoate(1) + <i>n</i> -heptane(2)					
288.15 K					
0.8972	1014.2	-0.201	1.904	-0.290	-0.136
0.7984	978.6	-0.281	1.532	-0.469	-0.258
0.6974	942.0	-0.316	1.250	-0.553	-0.336
0.5985	906.1	-0.317	1.041	-0.569	-0.374
0.4961	868.8	-0.289	0.868	-0.542	-0.394
0.3941	831.7	-0.239	0.733	-0.478	-0.385
0.2948	795.6	-0.177	0.625	-0.392	-0.362
0.1952	759.6	-0.112	0.547	-0.275	-0.277
0.0980	724.6	-0.051	0.490	-0.143	-0.148
298.15 K					
0.8972	1005.0	-0.196	1.539	-0.211	-0.132
0.7984	969.3	-0.314	1.263	-0.338	-0.238
0.6974	932.6	-0.375	1.047	-0.401	-0.309
0.5985	896.5	-0.387	0.882	-0.417	-0.347
0.4961	859.1	-0.360	0.747	-0.398	-0.362
0.3941	821.8	-0.305	0.638	-0.353	-0.354
0.2948	785.6	-0.232	0.550	-0.290	-0.333
0.1952	749.5	-0.151	0.484	-0.205	-0.257
0.0980	714.4	-0.072	0.428	-0.115	-0.183
308.15 K					
0.8972	995.7	-0.218	1.286	-0.150	-0.107
0.7984	960.2	-0.351	1.082	-0.234	-0.175
0.6974	923.5	-0.423	0.912	-0.282	-0.230
0.5985	887.4	-0.442	0.767	-0.308	-0.297
0.4961	850.0	-0.418	0.655	-0.296	-0.310
0.3941	812.8	-0.362	0.564	-0.265	-0.307
0.2948	776.7	-0.285	0.492	-0.216	-0.274
0.1952	740.7	-0.193	0.433	-0.155	-0.221
0.0980	705.6	-0.097	0.387	-0.084	-0.139
318.15 K					
0.8972	986.3	-0.226	1.080	-0.114	-0.101
0.7984	950.8	-0.373	0.913	-0.184	-0.181
0.6974	914.2	-0.462	0.771	-0.227	-0.254
0.5985	878.3	-0.469	0.662	-0.240	-0.292
0.4961	841.0	-0.483	0.571	-0.232	-0.305
0.3941	803.9	-0.431	0.498	-0.205	-0.285
0.2948	767.9	-0.350	0.440	-0.166	-0.241
0.1952	731.9	-0.245	0.393	-0.116	-0.169
0.0980	696.9	-0.127	0.351	-0.063	-0.108

flow, obtained using

$$\Delta g^{*E} = RT(\ln \eta v - x_1 \ln \eta_1 v_1 - x_2 \ln \eta_2 v_2) \quad (1)$$

where v is the molar volume and η is the dynamic viscosity of the mixture, and the subscripts refer to the pure components; R is the universal gas constant, and T is absolute temperature. The excess magnitudes, here represented generically by Y^E , were correlated using the polynomial equation

$$Y^E = x_1 x_2 \sum_{i=0}^n A_i z^i \quad (2)$$

where

$$z = x_1 / (x_1 + kx_2) \quad (3)$$

The A_i coefficients were calculated in each case using a least-squares method to find the value of k that minimized the standard deviation $s(Y^E)$ between the experimental data and eqn. (2). Table 3 presents the values thus obtained. Figures 1(a) and 1(b) depict the curves for v^E and η^E for the different cases of the two systems studied.

As mentioned in the introduction, the literature contains v^E values for the two mixtures (methyl benzoate or ethyl benzoate + n -heptane) at 298.15 K. Figure 2 shows the differences between these data and our v^E data fitted by eqn. (2). The mean error between our data and the values reported by Grolier et al. [2] was 39% for the mixture methyl benzoate + n -heptane and 30.6% for the mixture ethyl benzoate + n -heptane; the mean error with respect to the values reported by Dussart et al. [3] was 22.3% for methyl benzoate + n -heptane and 22.2% for ethyl benzoate + n -heptane.

Viscosity may be related to the thermodynamic activation magnitudes for the mixtures using the equation of Eyring et al. [8]

$$\eta = \frac{hN}{v} \exp[\Delta h^\ddagger / RT - \Delta s^\ddagger / R] \quad (4)$$

from which the thermodynamic activation values Δh^\ddagger and Δs^\ddagger can be calculated. It follows that Δg^\ddagger can then be obtained, because $\Delta g^\ddagger = \Delta h^\ddagger - T \Delta s^\ddagger$. These values appear in Table 3.

DISCUSSION

The qualitative representations of the excess magnitudes v^E and η^E presented in Figs. 1(a) and (b) reveal certain important characteristics of mixtures of alkyl benzoate + n -heptane. Firstly, higher volumetric contractions could be expected in these mixtures as compared to those in mixtures with n -nonane [1]: the possibility of interstitial accommodation of the

TABLE 3

Coefficients k , A_i and standard deviations obtained for eqn. (2)

T/K	k	A_0	A_1	A_2	A_3	$s(Y^E)$
Methyl benzoate + <i>n</i>-heptane						
$v^E \times 10^6 / (\text{m}^3 \text{mol}^{-1})$						
288.15	0.998	0.091	-2.271	-	-	0.0054
298.15	1.127	-0.135	-2.433	-	-	0.0067
308.15	3.046	-0.154	-8.487	14.305	-9.926	0.0034
318.15	3.005	-0.350	-8.285	13.594	-9.550	0.0057
$\eta^E / (\text{mPa s})$						
288.15	2.268	-1.441	-2.296	-	-	0.0048
298.15	3.079	-1.145	-1.764	-	-	0.0031
308.15	3.716	-0.906	-1.429	-	-	0.0043
318.15	1.941	-0.663	-0.824	-	-	0.0012
$\Delta g^{*E} / (\text{kJ mol}^{-1})$						
288.15	0.190	-1.990	-	-	-	0.0127
298.15	0.597	-2.440	2.039	-1.659	-	0.0117
308.15	2.900	-1.834	1.139	-1.836	-	0.0120
318.15	0.190	-1.570	-	-	-	0.0059
Ethyl benzoate + <i>n</i>-heptane						
$v^E \times 10^6 / (\text{m}^3 \text{mol}^{-1})$						
288.15	3.084	-0.446	-3.997	5.436	-4.327	0.0051
298.15	1.090	-0.664	-1.638	-	-	0.0059
308.15	1.256	-0.974	-1.592	-	-	0.0047
318.15	1.056	-1.325	-1.260	-	-	0.0055
$\eta^E / (\text{mPa s})$						
288.15	2.217	-1.534	-2.101	-	-	0.0040
298.15	2.454	-1.179	-1.468	-	-	0.0029
308.15	1.954	-0.896	-0.850	-	-	0.0028
318.15	1.379	-0.640	-0.688	-	-	0.0010
$\Delta g^{*E} / (\text{kJ mol}^{-1})$						
288.15	0.342	-1.876	0.361	-	-	0.0094
298.15	0.144	-3.446	4.190	-2.201	-	0.0064
308.15	0.412	-1.634	0.574	-	-	0.0079
318.15	0.190	-1.183	-	-	-	0.0090

hydrocarbon molecules among the ester molecules increases with decreasing *n*-alkane chain length. However, the v^E values became more negative as the number of carbon atoms in the benzoate increases, resulting in lower polarity and a weakening of the associations between ester molecules, thereby enabling induced dipole–dipole complexes to form between the benzoate and the *n*-heptane, which in turn gave rise to endothermic effects

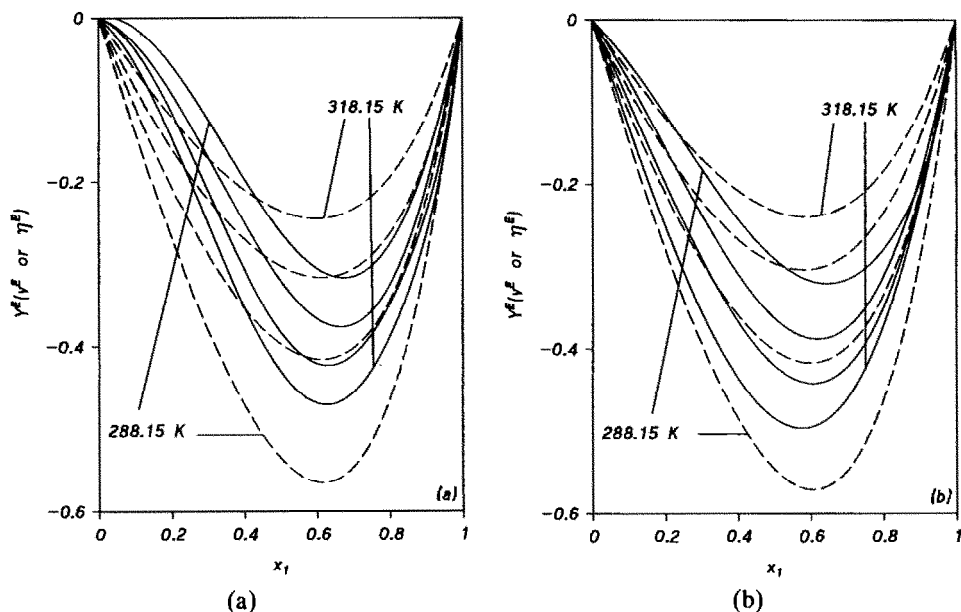


Fig. 1. —, Excess molar volumes $v^E \times 10^6 / (\text{m}^3 \text{mol}^{-1})$ and ---, excess viscosities $\eta^E / (\text{mPa s})$ for the binary systems (a) x_1 methyl benzoate + x_2 *n*-heptane and (b) x_1 ethyl benzoate + x_2 *n*-heptane, as a function of temperature.

in the mixing process [2]. The contraction in the volume increased significantly as temperature increased.

However, the η^E and Δg^{*E} values became less negative as the temperature rose; this behavior was similar to that in the system studied previously [1]. Because of the above arguments and in accordance with the Arrhenius theory, the negative values of the activation entropies (Table 4)

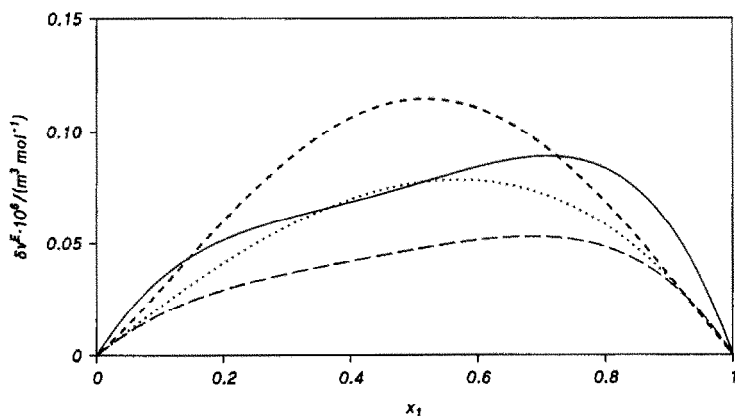


Fig. 2. Deviations $\delta v^E = (v^E - v_{\text{cal}}^E)$ from eqn. (2) of the values obtained by other authors at 298.15 K for the mixture x_1 methyl benzoate + x_2 *n*-heptane: —, Grolier et al. [2]; — — —, Dusart et al. [3]; and for x_1 ethyl benzoate + x_2 *n*-heptane: ---, Grolier et al. [2]; \cdots , Dusart et al. [3].

TABLE 4

Activation parameters for x_1 methyl (or ethyl) benzoate + x_2 *n*-heptane

x_1	$\Delta g^\ddagger / (\text{kJ mol}^{-1})$				$\Delta s^\ddagger / (\text{J K}^{-1} \text{mol}^{-1})$	$\Delta h^\ddagger / (\text{kJ mol}^{-1})$
	288.15	298.15	308.15	318.15		
Methyl benzoate(1) + <i>n</i> -heptane(2)						
1.0000	65.3	67.1	68.9	70.6	-176.4	14.5
0.9017	64.8	66.6	68.4	70.1	-178.7	13.3
0.8033	64.3	66.1	67.9	69.8	-180.9	12.2
0.6984	63.8	65.7	67.5	69.3	-183.4	11.0
0.5978	63.4	65.3	67.1	69.0	-185.3	10.0
0.5004	63.1	65.0	66.8	68.7	-185.8	9.6
0.3974	62.7	64.6	66.5	68.4	-188.0	8.6
0.3001	62.5	64.3	66.2	68.1	-187.8	8.4
0.1960	62.2	64.1	66.0	67.9	-189.8	7.5
0.0999	62.0	63.9	65.8	67.7	-189.7	7.3
0.0000	61.8	63.7	65.6	67.5	-189.2	7.3
Ethyl benzoate(1) + <i>n</i> -heptane(2)						
1.0000	65.6	67.3	69.1	70.9	-175.8	14.9
0.8972	65.0	66.8	68.6	70.4	-179.3	13.3
0.7984	64.6	66.4	68.2	70.0	-181.4	12.3
0.6974	64.1	65.9	67.8	69.6	-183.1	11.3
0.5985	63.7	65.5	67.4	69.2	-184.1	10.6
0.4961	63.3	65.1	67.0	68.8	-185.7	9.8
0.3941	62.9	64.8	66.6	68.5	-187.3	8.9
0.2948	62.5	64.4	66.3	68.2	-189.5	7.9
0.1952	62.3	64.2	66.1	68.0	-190.2	7.5
0.0980	62.0	63.9	65.8	67.7	-189.5	7.4
0.0000	61.8	63.7	65.6	67.5	-189.3	7.3

and the high Δh^\ddagger values suggest the existence of molecular interactions that give rise to a more rigid molecular arrangement.

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REFERENCES

- 1 B. Garcia, M.J. Miranda, J.M. Leal, J. Ortega and J.S. Matos, *Thermochim. Acta*, 186 (1991) 285.
- 2 J.P.E. Grolier, D. Ballet and A. Viillard, *J. Chem. Thermodyn.*, 6 (1974) 895.
- 3 O. Dusart, C. Piekarski, S. Piekarski and A. Viillard, *J. Chim. Phys.*, 73 (1976) 837.
- 4 J.A. Riddick, W.B. Bunger and T.K. Sakano, *Organic Solvents Techniques of Chemistry*, 4th edn., 1986, Wiley-Interscience, New York.

- 5 J. Ortega and J.S. Matos, *Mater. Chem. Phys.*, 15 (1986) 415.
- 6 T.R.C. *Thermodynamic Tables of Hydrocarbons*, Thermodynamic Research Center, Texas A&M University, 1973, pp. d-1011, c-k-1011.
- 7 J. Timmermans, *Physico-Chemical Constants of Pure Organic Compounds*, Vol. 2, Elsevier, Amsterdam, 1976.
- 8 H. Eyring, R.E. Powell and W.E. Roseware, *Ind. Eng. Chem.*, 33 (1941) 837.